

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing tetrahydrogeranylacetone, comprising, ~~conducting~~ passing a liquid phase, comprising at least 90% by weight of pseudoionone and in which particles of a catalyst which is capable of preferentially hydrogenating carbon-carbon double bonds over carbon-oxygen double bonds, and the active component of which comprises palladium are suspended, through a device which inhibits the transport of the catalyst particles in the presence of a hydrogen-containing gas.

Claim 2 (Previously Presented): A process as claimed in claim 1, wherein the device inhibiting the transport of the catalyst particles has orifices or channels whose hydraulic diameter is from 2 to 2000 times the average diameter of the catalyst particles.

Claim 3 (Previously Presented): A process as claimed in claim 1, wherein catalyst particles having an average diameter of from 0.0001 to 2 mm are used.

Claim 4 (Previously Presented): A process as claimed in claim 1, wherein the device used for inhibiting the transport of the catalyst particles is a dumped packing, a knit, an open-celled foam structure or a structured packing element.

Claim 5 (Previously Presented): A process as claimed in claim 1, wherein the liquid phase and the hydrogen-containing gas are conducted through the device which inhibits the transport of the catalyst particles at a superficial velocity of more than $100 \text{ m}^3/\text{m}^2\text{h}$.

Claim 6 (Previously Presented): A process as claimed in claim 1, wherein the surfaces of the device facing toward the liquid phase have a roughness in the range from 0.1 to 10 times the average diameter of the catalyst particles.

Claim 7 (Previously Presented): A process as claimed in claim 1, wherein the reaction pressure is from 1 to 100 bar.

Claim 8 (Previously Presented): A process as claimed in claim 1, wherein the reaction temperature is from 20 to 120°C.

Claims 9-10 (Canceled).

Claim 11 (New): A process for making tetrahydrogeranylacetone, comprising:
hydrogenating, in the liquid phase, the carbon-carbon double bonds of pseudoionone without hydrogenating the carbon-oxygen double bonds of the pseudoionone,
wherein the hydrogenating is carried out by contacting a hydrogen-containing gas with a mixture comprising at least 90% by weight of pseudoionone,
wherein the mixture further comprises a catalyst having an active component comprising palladium, and
wherein during the hydrogenating the active component is suspended by a device that inhibits transport of particles of the catalyst.

Claim 12 (New): The process as claimed in claim 11, wherein the device inhibiting the transport of particles of the catalyst has at least one of a plurality of orifices and a

plurality of channels, wherein the orifices and the channels have a hydraulic diameter of from 2 to 2,000 times the average diameter of the particles of the catalyst.

Claim 13 (New): The process as claimed in claim 11, wherein the particles of the catalyst have an average diameter of from 0.0001 to 2 mm.

Claim 14 (New): The process as claimed in claim 1, wherein the device used to inhibit transport of the particles of the catalyst is a dumped packing, a knit, an open-celled film structure or a structured packing element.

Claim 15 (New): The process as claimed in claim 11, wherein the mixture phase and the hydrogen-containing gas are conducted through the device to inhibit transport of particles of the catalyst,

wherein the hydrogenating is carried out at a superficial velocity of more than 100 $\text{m}^3/\text{m}^2\text{k}$.

Claim 16 (New): The process as claimed in claim 11, wherein the device has one or more surfaces contacting the mixture and having a roughness in the range of from 0.1 to 10 times the average diameter of the particles of the catalyst.

Claim 17 (New): The process as claimed in claim 11, wherein a reaction pressure is from 1 to 100 bar.

Claim 18 (New): The process as claimed in claim 11, wherein a reaction temperature is from 20 to 120°C.

Claim 19 (New): The process as claimed in claim 1, wherein the liquid phase is essentially free of diluents.

Claim 20 (New): The process as claimed in claim 1, wherein the liquid phase and the gas phase leaving the device are partially recycled to the device.

Claim 21 (New): The process as claimed in claim 11, wherein the mixture comprises no diluents.

Claim 22 (New): The process as claimed in claim 11, wherein a portion of the mixture and a portion of a gas phase leaving the device are partially recycled to the device.

Claim 23 (New): The process as claimed in claim 1, wherein more than 96% of the psuedoionone is hydrogenated to selectively form tetrahydrogeranylacetone.

Claim 24 (New): The process as claimed in claim 11, wherein more than 96% of the psuedoionone is hydrogenated to selectively form tetrahydrogeranylacetone.

Claim 25 (New): The process as claimed in claim 23, wherein more than 99.9% of the psuedoionone is hydrogenated.

Claim 26 (New): The process as claimed in claim 24, wherein more than 99.9% of the psuedoionone is hydrogenated.

DISCUSSION OF THE AMENDMENT

Claims 1-8 and 11-26 are active in the present application. Claims 9-10 are canceled claims. Claim 1 is amended for clarity. Claims 11-26 are new claims. Support for the new claims is found in the original claims. Support for new Claims 19 and 21 is found in paragraph [0020] of the PG publication corresponding with the present application (i.e., 2006/0211898). Support for new Claims 20 and 22 is found in paragraphs [0026] of the PG publication. Support for new Claims 23-26 is found on page 7, last two paragraphs.

No new matter is added.